# Dissolving driven by vigorous compositional convection 

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The one-dimensional dissolution that occurs when a binary melt is placed above or below a solid of a different composition is examined both theoretically and experimentally. In the case considered, the dissolution is driven by vigorous compositional convection that results from a Rayleigh-Bénard instability of the compositional boundary layer in the vicinity of the dissolving solid. A scaling analysis is used to derive theoretical expressions for both the dissolving velocity and the interfacial fluid concentration. Laboratory experiments are also described in which ice is dissolved when it is overlain or underlain by aqueous solutions. The measured dissolving velocities are consistent with the theoretical expressions, and yield estimates of the critical Rayleigh number for boundary-layer instability. The results of this study are then applied to predict the rate at which dissolution will occur when undersaturated mixed magmas are generated during the periodic replenishment of large basaltic magma chambers in the Earth's crust.

## 1. Introduction

Both the melting and the dissolving of solids in fluids are fundamental physical phenomena which are encountered daily; for example, whenever ice is melted in water or sugar dissolved in coffee. Melting occurs when the temperature of the fluid is significantly greater than the melting temperature of the solid, and is controlled by thermal diffusion (cf. Woods 1992; Kerr 1994; and the Appendix). In contrast, dissolving occurs at relatively lower fluid temperatures, and is due to chemical disequilibrium between the solid and fluid. It is controlled by compositional diffusion and will continue for as long as the fluid remains above its freezing temperature.

In the special case where both the thermal and compositional fields in the fluid are gravitationally stable, fluid mechanics does not play a role, and the rate at which either melting or dissolving occurs can be determined analytically (Woods 1992). Often however, either or both of the thermal and compositional fields will be unstable and convection will result. Convection invariably enhances the rate of melting or dissolving by assisting the transfer of heat and composition to the solid. Recent studies have quantified this rate in the one-dimensional cases of melting driven by forced turbulent flow (Huppert 1989), free thermal convection (Huppert \& Sparks 1988a, b) and free compositional convection (Kerr 1994). In the latter case, compositional convection arises when a hot fluid melts an underlying solid, and the density of the melted solid is less than that of the fluid, or when the hot fluid melts an overlying solid whose melt density is greater than that of the fluid.

The present paper is a natural continuation of the above studies, and quantifies the rate of dissolution of a horizontal boundary in the presence of vigorous compositional
convection. I begin in $\S 2$ by using a scaling analysis to derive theoretical expressions for the temperature, concentration and velocity of the interface. These expressions are then compared in $\S 3$ with the results of a series of experiments in which either an ice floor or roof is dissolved in contact with aqueous solutions. The results are applied to replenished magma chambers in $\S 4$, and then summarized in $\S 5$.

## 2. Scaling theory

### 2.1. Dissolving a floor

Consider the dissolving of a solid of composition $C_{s}$, melting temperature $T_{m}$ and farfield temperature $T_{s}$, overlain by a fluid with a composition $C_{f}$ and temperature $T_{f}$. If the volume of fluid is large, the far-field conditions will not change, and it is expected that the solid dissolves at a constant velocity $V$. The resulting thermal and compositional profiles are shown in figure 1 and illustrated on a typical phase diagram in figure 2. At the interface between the solid and the fluid, the temperature $T_{i}$ and composition $C_{i}$ are constrained thermodynamically to lie on the liquidus curve

$$
\begin{equation*}
T_{i}=T_{L}\left(C_{i}\right) \tag{1}
\end{equation*}
$$

which gives the freezing temperature of the fluid as a function of concentration. Within the solid, the temperature is given by

$$
\begin{equation*}
T(z)=T_{s}+\left(T_{i}-T_{s}\right) \mathrm{e}^{-V z / \kappa_{s}} \tag{2}
\end{equation*}
$$

(Carslaw \& Jaeger 1986), where $\kappa_{s}$ is the thermal diffusivity of the solid.
There are composition and thermal boundary layers immediately adjacent to the interface. If the respective fluxes to the interface through these layers are $F_{C}$ and $F_{T}$, the effective layer thicknesses can be defined by

$$
\begin{equation*}
F_{C}=\frac{D\left(C_{f}-C_{i}\right)}{h_{C}} \quad \text { and } \quad F_{T}=\frac{k_{f}\left(T_{f}-T_{i}\right)}{h_{T}} \tag{3a,b}
\end{equation*}
$$

where $D$ and $k_{f}$ are the compositional diffusivity and thermal conductivity of the fluid. If the volume change associated with the phase change is neglected (cf. Woods 1992; Chiareli, Huppert \& Worster 1994), the boundary-layer fluxes are also linked to the dissolving rate $V$ by the interfacial conditions

$$
\begin{equation*}
F_{C}=V\left(C_{i}-C_{s}\right) \quad \text { and } \quad F_{T}=V\left(\rho_{s} L_{s}+\rho_{s} c_{s}\left(T_{i}-T_{s}\right)\right) \tag{4a,b}
\end{equation*}
$$

where $\rho_{s}, L_{s}$ and $c_{s}$ are the density, latent heat and specific heat of the solid.
The aim is to use scaling theory to determine $V$ in the case where dissolving of the solid leads to vigorous compositional convection, a situation which will occur if the density $\rho_{i}$ of the fluid at the interface is sufficiently less than the density $\rho_{f}$ of the farfield fluid. I assume that the interface between the solid and the fluid is flat, and that the unstable compositional buoyancy released at the interface dominates the stabilizing thermal buoyancy, i.e. that the ratio $\mathscr{R}$ of these buoyancies satisfies the condition

$$
\begin{equation*}
\mathscr{R} \equiv \frac{\beta\left(C_{f}-C_{s}\right)}{\alpha\left[\rho_{s} L_{s}+\rho_{s} c_{s}\left(T_{i}-T_{s}\right)\right] / \rho_{f} c_{f}} \gg 1 \tag{5}
\end{equation*}
$$

where $\alpha$ is the coefficient of thermal expansion and $\beta$ is the equivalent coefficient for the variation of density with composition.


Figure 1. The thermal and compositional profiles when a solid dissolves into a fluid at velocity $V$.


Figure 2. The path on a simple phase diagram of the thermal and compositional profiles shown in figure 1 . The dotted portion of the path represents the jump in composition at the dissolving interface.

Accordingly, it is envisaged that both the compositional and thermal boundary layers grow diffusively with time $t$ :

$$
\begin{equation*}
h_{C} \sim(D t)^{1 / 2}, \quad h_{T} \sim\left(\kappa_{f} t\right)^{1 / 2} \tag{6a,b}
\end{equation*}
$$

where $c_{f}$ and $\kappa_{f} \equiv k_{f} / \rho_{f} c_{f}$ are the specific heat and thermal diffusivity of the fluid, until a time $\tau$ when the buoyant compositional boundary layer undergoes a Rayleigh-Bénard type of instability that drives vigorous compositional convection. Following Lick (1965) and Howard (1966), instability can be expected when the Rayleigh number $R a$ of this boundary layer reaches a critical value $R a_{c}$ :

$$
\begin{equation*}
R a_{c}=\frac{g\left(\rho_{f}-\rho_{i}\right) h_{C}^{3}}{D \mu} \tag{7}
\end{equation*}
$$

where $g$ is the acceleration due to gravity and $\mu$ is the fluid viscosity. I therefore obtain the estimates

$$
\begin{equation*}
h_{C}=\left(\frac{R a_{c} D \mu}{g\left(\rho_{f}-\rho_{i}\right)}\right)^{1 / 3}, \quad h_{T}=h_{C}\left(\frac{\kappa_{f}}{D}\right)^{1 / 2}=\left(\frac{R a_{c}^{2} \mu^{2} \kappa_{f}^{3}}{D g^{2}\left(\rho_{f}-\rho_{i}\right)^{2}}\right)^{1 / 6}, \quad \tau \approx\left(\frac{R a_{c}^{2} \mu^{2}}{D g^{2}\left(\rho_{f}-\rho_{i}\right)^{2}}\right)^{1 / 3} . \tag{8a-c}
\end{equation*}
$$

Substitution of ( $8 a$ ) and ( $3 a$ ) into ( $4 a$ ) then yields the prediction that the dissolving velocity is

$$
\begin{equation*}
V=\left(\frac{g\left(\rho_{f}-\rho_{i}\right) D^{2}}{R a_{c} \mu}\right)^{1 / 3}\left(\frac{C_{f}-C_{i}}{C_{i}-C_{s}}\right) \tag{9}
\end{equation*}
$$

while combining (9), $(8 b),(3 b),(4 b)$ and (1) shows that

$$
\begin{equation*}
T_{f}-T_{L}\left(C_{i}\right)=\frac{\rho_{s} L_{s}+\rho_{s} c_{s}\left(T_{L}\left(C_{i}\right)-T_{s}\right)}{\rho_{f} c_{f}}\left(\frac{D}{\kappa_{f}}\right)^{1 / 2}\left(\frac{C_{f}-C_{i}}{C_{i}-C_{s}}\right) \tag{10}
\end{equation*}
$$

From the above analysis, it is concluded that the dissolving rate is given by (9), once $C_{i}$ is evaluated from (10). I also note that $R a_{c}^{-1 / 3}$ is equivalent to the constant $\gamma$ in the semi-empirical expression $N u=\gamma R a^{1 / 3}$ that relates the Nusselt number to the Rayleigh number, and is in general a function of the Prandtl number and the aspect ratio of the convecting region (Turner 1979; Denton \& Wood 1979; Davaille \& Jaupart 1993).

In the above analysis, it has been implicitly assumed that the distance $(D \tau)^{1 / 2}$ over which compositional diffusion occurs is large in comparison with the distance $V \tau$ that the solid has dissolved in the time $\tau$ for instability. From ( $8 a$, , ( $8 c$ ) and (9), it is found that
where

$$
\begin{align*}
& V \tau \approx h_{C} / \mathscr{C}  \tag{11}\\
& \mathscr{C} \equiv \frac{C_{i}-C_{s}}{C_{f}-C_{i}} \tag{12}
\end{align*}
$$

Equations (9) and (10) are therefore asymptotically correct when $\mathscr{C} \gg 1$, a condition that is closely analogous to the condition that the Stefan number is large during melting driven by vigorous compositional convection (see Kerr 1994). If $\mathscr{C}$ is smaller however (i.e. $\mathscr{C} \gtrsim 1$ ), then (11) suggests that $h_{C}$ is more accurately estimated by

$$
\begin{equation*}
h_{C}=\left(\frac{R a_{c} D \mu}{g\left(\rho_{f}-\rho_{i}\right)}\right)^{1 / 3}\left(1+\frac{1}{\mathscr{C}}\right), \tag{13}
\end{equation*}
$$

which results in $V$ and $T_{f}-T_{i}$ being given by

$$
\begin{gather*}
V=\left(\frac{g\left(\rho_{f}-\rho_{i}\right) D^{2}}{R a_{c} \mu}\right)^{1 / 3}\left(\frac{C_{f}-C_{i}}{C_{f}-C_{\delta}}\right)  \tag{14}\\
T_{f}-T_{i}\left(C_{i}\right)=\frac{\rho_{s} L_{s}+\rho_{s} c_{s}\left(T_{L}\left(C_{i}\right)-T_{s}\right)}{\rho_{f} c_{f}}\left(\frac{D}{\kappa_{f}}\right)^{1 / 2}\left(\frac{C_{f}-C_{i}}{C_{f}-C_{s}}\right) . \tag{15}
\end{gather*}
$$

and
The presence of $D$ in (14) reflects the fact that dissolution is primarily dependent on the diffusion of composition. The dependence on the diffusion of heat enters only weakly through (15), and in the limit of $D / \kappa_{f} \rightarrow 0$, then $T_{i} \rightarrow T_{f}, C_{i} \rightarrow C_{L} \equiv T_{L}^{-1}\left(T_{f}\right)$ (see figure 2), $\rho_{i} \rightarrow \rho_{L} \equiv \rho_{f}\left(C_{L}, T_{f}\right)$ and the dissolution is entirely due to compositional diffusion:

$$
\begin{equation*}
V=\left(\frac{g\left(\rho_{f}-\rho_{L}\right) D^{2}}{R a_{c} \mu}\right)^{1 / 3}\left(\frac{C_{f}-C_{L}}{C_{f}-C_{s}}\right) \tag{16}
\end{equation*}
$$

This control by compositional diffusion breaks down, however, when $\mathscr{C} \ll 1$. In this important limit where dissolving undergoes a transition to melting, the compositional profile becomes very nonlinear, equation ( $3 a$ ) is no longer accurate, and a new scaling analysis is required (which is presented in the Appendix).

### 2.2. Dissolving a roof

In the case of dissolving a roof, compositional convection will occur if the density of the interfacial fluid is greater than that of the far-field fluid. The dissolving rate will be given by (14) and (15), with $\rho_{f}-\rho_{i}$ replaced by $\rho_{i}-\rho_{f}$, provided that the unstable compositional buoyancy is much greater than the unstable thermal buoyancy ( $\not \subset \ngtr 1$ ). In opposite limit, $\mathscr{R} \ll 1$, the heat transfer to the dissolving interface will be driven by thermal convection. The thickness of the thermal boundary layer is then no longer given by ( $8 b$ ), but by

$$
\begin{equation*}
h_{T}=\left(\frac{R a_{c} \mu \kappa_{f}}{g \rho_{f} \alpha\left(T_{f}-T_{i}\right)}\right)^{1 / 3}, \tag{17}
\end{equation*}
$$

which leads to the temperature difference (15) being replaced by the smaller value

$$
\begin{equation*}
T_{f}-T_{L}\left(C_{i}\right)=\frac{\rho_{s} L_{s}+\rho_{s} c_{s}\left(T_{L}\left(C_{i}\right)-T_{s}\right)}{\rho_{f} c_{f}}\left(\frac{D}{\kappa_{f}}\right)^{1 / 2}\left(\frac{C_{f}-C_{i}}{C_{f}-C_{s}}\right) \mathscr{R}^{1 / 4} . \tag{18}
\end{equation*}
$$

## 3. Experiments

In this section two series of experiments are described that were performed to test the scaling analysis presented in $\S 2$. In these experiments, either an ice roof or an ice floor was dissolved by contact with an aqueous solution.

### 3.1. Roof experiments ( $R$ )

In these experiments, a block of bubble-free ice, $20 \times 20 \mathrm{~cm}^{2}$ in cross-section and 7 cm thick, was inserted into the top of an insulated glass tank to leave a space underneath that was $20 \times 20 \mathrm{~cm}^{2}$ in cross-section and 53 cm high. An aqueous solution of isopropanol was then added through a hole in the base of the tank until it made contact with the ice. The isopropanol solution was used because its density is less than that of water, and because the anomalous density maximum at $4^{\circ} \mathrm{C}$ that is associated with pure water can be eliminated by using a sufficient concentration of isopropanol (Kerr et al. 1990).

Five experiments were performed, with far-field concentrations of isopropanol which ranged from 22 to $36.5 \mathrm{wt} \%$ (see table 1). For these values, which are illustrated on the phase diagram in figure 3 , the unstable compositional buoyancy is much greater than the unstable thermal buoyancy $(\mathscr{R} \gg 1)$ and the solution convected vigorously. In all the experiments, the far-field temperature was $-6.2 \pm 0.5^{\circ} \mathrm{C}$, which corresponds to a liquidus concentration $C_{L}$ of $16.8 \pm 0.8 \mathrm{wt} \%$.

Direct observations of the experiments were supplemented by both photographs and videos. These observations showed that the surface of the dissolving ice was pitted. It was also found that the presence of any air bubbles at the ice interface led to the growth of conical cavities in the ice. This interesting phenomenon has also been observed during the melting of an ice roof and is not well understood (Kerr 1994, §4.3 and figure 8 ).

Observations of the thickness of the ice block as a function of time demonstrated


Figure 3. Experimental measurements (from Washburn 1926) of the freezing temperature for aqueous solutions of isopropanol. The far-field conditions of the five experiments are indicated by $\times$.

| Quantity | R1 | R2 | R3 | R4 | R5 | Units | Source |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| $C_{f}$ | 36.5 | 33 | 32 | 27 | 22 | wt \% |  |
| $\rho_{f}$ | 0.954 | 0.961 | 0.9635 | 0.972 | 0.978 | $\mathrm{g} \mathrm{cm}^{-3}$ | A, C |
| $c_{j}$ | 4.15 | 4.29 | 4.33 | 4.48 | 4.57 | $\mathrm{J} \mathrm{g}^{-1} \mathrm{~cm}^{-1}$ | A |
| $k_{f}$ | 0.346 | 0.364 | 0.369 | 0.396 | 0.424 | $\mathrm{W} \mathrm{m} \mathrm{m}^{-1}{ }^{\circ} \mathrm{C}^{-1}$ | B |
| $\nu_{f}$ | 19.0 | 17.5 | 17.1 | 15.0 | 12.9 | $\mathrm{mm}^{2} \mathrm{~s}^{-1}$ | C |
| $C_{i}$ | 19.7 | 19.3 | 19.2 | 18.5 | 17.8 | wt \% |  |
| $T_{i}$ | -8.1 | -7.8 | -7.7 | -7.3 | -6.9 | ${ }^{\circ} \mathrm{C}$ |  |
| $\rho_{i}$ | 0.9784 | 0.9788 | 0.9789 | 0.9797 | 0.9805 | $\mathrm{g} \mathrm{cm}^{-3}$ |  |
| $\mathscr{C}$ | 1.2 | 1.4 | 1.5 | 2.2 | 4.3 | - |  |
| $\mathscr{R}$ | 4.4 | 3.9 | 3.6 | 2.8 | 2.2 | - |  |
| $\mathscr{F}$ | 4.32 | 3.60 | 3.35 | 2.20 | 1.02 | $\mu \mathrm{m} \mathrm{s}^{-1}$ |  |
| $V_{\text {expt }}$ | 1.30 | 1.23 | 1.08 | 0.58 | 0.37 | $\mu \mathrm{m} \mathrm{s}^{-1}$ |  |
| $\mathscr{V} / V_{\text {expt }}$ | 0.30 | 0.34 | 0.32 | 0.26 | 0.37 |  |  |

Table 1. Experimental parameters and results for the dissolving of an ice roof. All the experiments used aqueous solutions of isopropanol at $T_{f}=-6.2{ }^{\circ} \mathrm{C}$ and ice at $T_{s}=-9{ }^{\circ} \mathrm{C} . \mathscr{\gamma}, T_{i}$ (in ${ }^{\circ} \mathrm{C}$ ) and $C_{i}$ (in wt \% isopropanol) were found using (15) and (19) given the approximate liquidus relationship $T_{i}=-6.2+0.65\left(C_{i}-16.8\right)$ (see (3.22) of Kerr et al. 1990). The physical properties of the solutions were obtained from: (A) Washburn (1926), (B) Vargaftik (1975) and (C) direct measurement of $\rho_{f}$ and $\nu_{f}=\mu_{f} / \rho_{f}$ using calibrated viscometers and hydrometers. Other parameters used are $\rho_{s} L_{s}=306 \mathrm{~J} \mathrm{~cm}^{-3}$ (Washburn 1926), $\rho_{s} c_{s}=1.832 \mathrm{~J} \mathrm{~cm}^{-3}$ (Weast 1989), $\alpha=1.35 \times 10^{-4}{ }^{\circ} \mathrm{C}^{-1}$ (Kerr et al. 1990) and $D=0.24 \times 10^{-5} \mathrm{~cm}^{2} \mathrm{~s}^{-1}$ (Washburn 1926; Gary-Bobo \& Weber 1969).
that the block dissolved at a constant velocity (figure 4). The dissolving velocities are listed in table 1 , and are accurate to about $10 \%$. Also given in the table are values of $T_{i}$ and $C_{i}$ determined from (1) and (15), and values of the velocity scale $\mathscr{V}$ defined by

$$
\begin{equation*}
\mathscr{V}=\left(\frac{g\left(\rho_{f}-\rho_{i}\right) D^{2}}{\mu}\right)^{1 / 3}\left(\frac{C_{f}-C_{i}}{C_{f}-C_{s}}\right) . \tag{19}
\end{equation*}
$$

The error in determining $\mathscr{V}$ is about $20 \%$, and is principally due to uncertainties in $D$ and to small variations in $T_{f}$ during an experiment that lead to small variations in $C_{i}$.


Figure 4. The thickness $h$ of the ice block as a function of time during experiment R1. The results show that the melting velocity is constant throughout the experiment.


Figure 5. The dissolving velocities $V_{\text {expt }}$ (in $\mu \mathrm{m} \mathrm{s}^{-1}$ ) of an ice roof, in comparison with the velocity scale $\mathscr{V}$ defined by (19). The values lie on a straight line with a constant of proportionality of $0.320 \pm 0.040$.

The dissolving velocities, when plotted against $\mathscr{V}$ in figure 5 , are consistent with a straight line whose slope $R a_{c}^{-1 / 3} \approx 0.320 \pm 0.040$.

### 3.2. Floor experiments $(F)$

These experiments used a $20 \times 20 \times 20 \mathrm{~cm}^{3}$ Perspex tank with a metal base through which cold fluid was pumped. A block of bubble-free ice, about 3 cm thick, was first grown in the base of the tank. An experiment was then started by filling the rest of the tank with an aqueous solution of NaCl . The temperatures and compositions of the solutions are listed in table 2, and are shown on the $\mathrm{NaCl}-\mathrm{H}_{2} \mathrm{O}$ phase diagram in figure 6. The solution concentrations are accurate to within $0.1 \mathrm{wt} \%$, while the solution temperatures were kept constant to within $0.2^{\circ} \mathrm{C}$ by small additions of hot solution during an experiment.

In each of the experiments, vigorous compositional convection was observed. The vigorous convection is due to the buoyancy ratio $\mathscr{R}$ being significantly larger (see table 2) than the critical value of about 2.0 (Kerr 1994, figure 10). It is also noted that small solution concentrations do not lead to small values of $\mathscr{R}$ because these solutions have equally small coefficients of thermal expansion.

| Quantity | F1 | F2 | F3 | F4 | F5 | F6 | F7 | F8 | F9 | F10 |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| $T_{f}$ | -8.8 | -12.9 | -14.0 | -5.9 | -2.2 | -5.25 | -2.3 | 2.0 | 4.0 | 6.0 |
| $T_{s}$ | -9.4 | -14.8 | - 15.6 | - 15.6 | -8.4 | -9.6 | -7.6 | -11.0 | -11.0 | - 11.0 |
| ${ }_{\text {c }}$, | 22.0 | 23.2 | 23.0 | 22.2 | 21.68 | 16.5 | 15.3 | 19.3 | 19.5 | 20.35 |
| $p$, | 1.176 | 1.187 | 1.186 | 1.176 | 1.171 | 1.131 | 1.120 | 1.150 | 1.151 | 1.157 |
| $c_{f}$ | 3.33 | 3.30 | 3.30 | 3.33 | 3.35 | 3.46 | 3.50 | 3.40 | 3.40 | 3.38 |
| $k_{f}$ | 0.513 | 0.504 | 0.502 | 0.518 | 0.526 | 0.527 | 0.534 | 0.537 | 0.540 | 0.543 |
| $\nu_{f}$ | 3.33 | 4.06 | 4.23 | 3.00 | 2.57 | 2.57 | 2.26 | 2.13 | 2.02 | 1.95 |
| $\alpha$ | 3.4 | 3.2 | 3.1 | 3.6 | 3.8 | 3.0 | 3.0 | 3.8 | 4.0 | 4.2 |
| $C_{i}$ | 14.6 | 17.9 | 18.7 | 12.2 | 8.7 | 10.7 | 7.8 | 4.4 | 2.5 | 0.58 |
| $T_{i}$ | -10.5 | - 14.0 | -14.9 | -8.4 | -5.6 | -7.1 | - 5.0 | -2.7 | -1.5 | -0.35 |
| $\rho_{i}$ | 1.117 | 1.145 | 1.152 | 1.098 | 1.068 | 1.085 | 1.061 | 1.034 | 1.018 | 1.003 |
| $\mathscr{C}$ | 2.0 | 3.4 | 4.4 | 1.2 | 0.66 | 1.9 | 1.1 | 0.298 | 0.147 | 0.029 |
| $\mathscr{R}$ | 5.7 | 6.3 | 6.4 | 5.1 | 4.9 | 4.9 | 4.5 | 4.2 | 4.0 | 3.9 |
| $\mathscr{V}$ | 12.0 | 6.16 | 4.60 | 19.2 | 31.9 | 13.5 | 22.6 | 49.7 | 62.2 | 76.5 |
| $V_{\text {erpt }}$ | 3.15 | 1.42 | 1.08 | 4.30 | 7.38 | 3.25 | 4.70 | 9.82 | 13.0 | 15.7 |
| $\mathscr{Y}{ }^{\text {crpt }} V_{\text {expt }}$ | 0.27 | 0.23 | 0.24 | 0.22 | 0.23 | 0.24 | 0.21 | 0.20 | 0.21 | 0.21 |



Figure 6. The phase diagram for $\mathrm{H}_{2} \mathrm{O}-\mathrm{NaCl}$ (determined from experimental data given by Washburn 1926 and Weast 1989). The far-field conditions of the ten ice-floor experiments are indicated by $x$.


Figure 7. The dissolving velocities $V_{\text {expt }}$ (in $\mu \mathrm{m} \mathrm{s}^{-1}$ ) of an ice floor, in comparison with the velocity scale $\mathscr{V}$ defined by (19). The values lie on a straight line with a constant of proportionality of $0.226 \pm 0.022$.

All the experiments had pitted interfaces, as was also observed by Campbell (1986) and Fang \& Hellawell (1988, figure 3). In addition, a small number of larger hemispherical cavities were seen which are taken to be the 'cylindrical cavities' seen by Fang \& Hellawell (1988, figures 4 and 5). These cavities were irregularly distributed, infrequent, and probably arose from elongate air bubbles in the ice (Campbell 1986).

The dissolving velocities and the calculated velocity scale $\mathscr{V}$, which are both accurate to about $10 \%$, are plotted against each other in figure 7. The data are seen to lie on a straight line whose slope ( $0.226 \pm 0.022$ ) is lower than the value found in the roof experiments. The difference in these values probably reflects the fact that the roof experiments were somewhat accelerated by the release of a heat of solution (that was


Figure 8. The diopside-anorthite phase diagram, which was used by Campbell (1986) to demonstrate that mixing an anorthite-saturated magma (A) with a diopside-saturated magma (B) will result in a magma (C) that is undersaturated with respect to both anorthite and diopside. If this superheated magma is in contact with solid anorthite, the anorthite will be dissolved and the magma will chemically and thermally evolve (as shown by the arrowed path) until it is again on the liquidus (D).
about $25-40 \mathrm{~J} \mathrm{~g}^{-1}$ ) while the floor experiments were virtually unaffected by a $-3 \mathrm{~J} \mathrm{~g}^{-1}$ heat of solution that is negligible in comparison to the latent heat of the ice. Similar effects of a significant heat of solution have been found in experiments on melting driven by vigorous compositional convection (Kerr 1994, §4.1).

The value of 0.226 found above for $R a_{c}^{-1 / 3}$ can also be compared with values of about 0.16 found for $\gamma$ in careful measurements of the convective heat flux at high Rayleigh numbers in water (Katsaros et al. 1977) and diluted Golden Syrup (Davaille \& Jaupart 1993). The higher value obtained in the current experiments may be due to the larger surface area of the pitted dissolving boundary, which should enhance the diffusion of composition to it.

## 4. Geological application

One important situation where dissolving can be assisted by compositional convection is in large bodies of molten rock in the Earth's crust, which are generally referred to as 'magma chambers'. In some of these chambers, the resident magma cools, crystallizes and chemically evolves until it becomes saturated in the mineral plagioclase. Further cooling of the magma then leads to the growth of a plagioclaserich layer as the floor of the chamber. This steady evolution is frequently disrupted, however, by the fresh injection into the chamber of a new pulse of the parent magma (Huppert \& Sparks 1980). The new magma will typically be hotter, denser, and olivinesaturated, and it is usually input with sufficient momentum that a fountain results (Campbell \& Turner 1989). In the fountain, the replenishing and resident magmas are turbulently mixed to produce a magma that is not saturated with respect to either plagioclase or olivine (as is illustrated in figure 8 for the simple and well-known diopside-anorthite chemical system). This superheated magma is therefore able to dissolve the underlying plagioclase floor of the magma chamber.

### 4.1. The Bushveld Intrusion

Campbell (1986) proposed that considerable dissolution occurred immediately after a large replenishment during the formation of the 9 km thick Bushveld Igneous Intrusion in South Africa (Wager \& Brown 1968). In this replenishment, which immediately preceded the deposition of the platinum-rich Merensky Reef (Cameron 1982; Campbell, Naldrett \& Barnes 1983), it is envisaged that the input magma mixed with a resident magma to form a 1 km thick layer of superheated magma with a density $\rho_{f}$ of about $2.60 \mathrm{~g} \mathrm{~cm}^{-3}$ (Campbell \& Turner 1986, 1989). At the time of this replenishment, the floor of the magma chamber consisted of a thick plagioclase layer (with a composition of about $76 \mathrm{wt} \%$ anorthite and about $24 \mathrm{wt} \%$ albite) (Wager \& Brown 1968; Vermaak 1976; Eales et al. 1988). This anorthosite floor has a latent heat $\rho_{s} L_{8}$ of about $900 \mathrm{~J} \mathrm{~cm}^{-3}$ (Weill, Hon \& Navrotsky 1980; Stebbins, Carmichael \& Weill 1983) and a fractionation density $\rho_{f r}$ (i.e. the density of the components selectively added to the melt by dissolution of the crystals (Sparks \& Huppert 1984)) of about $2.50 \mathrm{~g} \mathrm{~cm}^{-3}$. Using also typical estimates (e.g. Huppert \& Sparks $1988 b$ ) of the thermal expansion coefficient ( $\alpha=5 \times 10^{-5}{ }^{\circ} \mathrm{C}^{-1}$ ) and heat capacity ( $c_{f}=1.34 \mathrm{~J}$ $\mathrm{g}^{-1}{ }^{\circ} \mathrm{C}^{-1}$ ) of the mixed magma, and neglecting the specific heat of the plagioclase in comparison to its latent heat (since its temperature will be only slightly less than that of the overlying magmas), the buoyancy ratio is estimated to be

$$
\begin{equation*}
\mathscr{R}=\frac{\rho_{f}-\rho_{f r}}{\alpha \rho_{s} L_{s} / c_{f}}=3.0 . \tag{20}
\end{equation*}
$$

This calculated ratio of the unstable compositional buoyancy to the stabilizing thermal buoyancy is larger than the critical value of about 2.0 that is necessary to sustain vigorous compositional convection (Kerr 1994).

Since the dissolution of the anorthosite was able to drive vigorous compositional convection, the theoretical and experimental results in this paper can be used to determine the rate at which it occurred. Equation (15) predicts that, for typical values of $D=10^{-8} \mathrm{~cm}^{2} \mathrm{~s}^{-1}$ (e.g. Hofmann 1980; Watson 1982; Zhang, Walker \& Lesher 1989; Van der Laan \& Wyllie 1993) and $\kappa_{f}=8 \times 10^{-3} \mathrm{~cm}^{2} \mathrm{~s}^{-1}$ (e.g. Huppert \& Sparks $1988 b$ ), the temperature difference $T_{f}-T_{i}$ (in units of ${ }^{\circ} \mathrm{C}$ ) is given by

$$
\begin{equation*}
T_{f}-T_{i}=0.3\left(\frac{C_{f}-C_{i}}{C_{f}-C_{s}}\right) \tag{21}
\end{equation*}
$$

This temperature difference is very small in comparison with the temperature variations in the phase diagram of the magma (as is indicated by figure 8), so that to a very good approximation $C_{i} \approx C_{L}$. Using (14) and estimating the magma viscosity $\mu$ as about $300 \mathrm{~g} \mathrm{~cm}^{-1} \mathrm{~s}^{-1}$, the predicted dissolving rate (in units of $\mathrm{m} \mathrm{y}^{-1}$ ) is given by

$$
\begin{equation*}
V=3.0\left(\frac{\rho_{f}-\rho_{L}}{R a_{c} \rho_{f}}\right)^{1 / 3}\left(\frac{C_{f}-C_{L}}{C_{f}-C_{s}}\right) \tag{22}
\end{equation*}
$$

From the floor dissolving experiments, $R a_{c}^{-1 / 3}$ has a value of about 0.226 . Hence for the magma C shown in figure 8 , for which $\left(\rho_{f}-\rho_{L}\right) / \rho_{f} \approx 0.01, C_{f}=68.3 \mathrm{wt} \%, C_{L}=$ $42.5 \mathrm{wt} \%$ and $C_{s}=0 \mathrm{wt} \%$, the dissolving velocity is initially

$$
\begin{equation*}
V=5.5 \mathrm{~cm} \mathrm{y}^{-1} \tag{23}
\end{equation*}
$$

which corresponds to initial boundary-layer thicknesses of about $h_{C}=0.35 \mathrm{~mm}$ and $h_{T}=31 \mathrm{~cm}$.

For comparison, it is noted that the dissolving velocity given by (23) is much greater than the probable solidification rate ( $\sim 0.1 \mathrm{~cm} \mathrm{y}^{-1}$ ) of the Bushveld intrusion (see Kerr \& Tait 1986), but is much smaller than the rate ( $3-20 \mathrm{~m} \mathrm{y}^{-1}$ ) at which a basaltic magma chamber can melt its roof (Huppert \& Sparks 1988a, $b$; Kerr 1994). The dissolution will cause a layer of magma $C$ of initial thickness $h=1 \mathrm{~km}$ to cool at a rate

$$
\begin{equation*}
\frac{\mathrm{d} T_{f}}{\mathrm{~d} t}=-\frac{V \rho_{s} L_{s}}{\rho_{f} c_{f} h} \approx 0.013^{\circ} \mathrm{C} \mathrm{y}^{-1} \tag{24}
\end{equation*}
$$

and to decrease in diopside content at a rate

$$
\begin{equation*}
\frac{\mathrm{d} C_{f}}{\mathrm{~d} t}=-\frac{V\left(\rho_{f} C_{f}-\rho_{s} C_{s}\right)}{\rho_{f} h} \approx 0.0037 \mathrm{wt} \% \mathrm{y}^{-1} \tag{25}
\end{equation*}
$$

This dissolution of the anorthosite continued until the vigorously convecting magma thermally and compositionally evolved to the point where it began to crystallize and deposit the Merensky Reef chromitite and pyroxenite.

It is important to note that the dissolving calculations above assume that the floor of the magma chamber is completely solid. In reality, however, the floor will be only partially solid, with a porosity that will vary with depth, and which will depend on the magma viscosity, the vigour of the convection, and the rate at which the chamber cools (Sparks et al. 1985; Campbell 1987). When the floor is porous, convective exchange can occur between the interstitial magma and the overlying mixed magma (Kerr \& Tait 1985). The convection takes the form of 'fingers' of dense magma that penetrate downwards into the porous medium with a velocity

$$
\begin{equation*}
V=0.55 \frac{k g\left(\rho_{U}-\rho_{L}\right)}{\epsilon \mu_{L}^{0.6} \mu_{U}^{0.4}} \tag{26}
\end{equation*}
$$

where $k$ is the permeability, $\epsilon$ is the porosity, and $L$ and $U$ refer to lower (interstitial) and upper (mixed) magmas respectively. For finger penetration to significantly accelerate dissolution, their velocity must be greater than the dissolving velocity given by (23), which will require a local floor porosity of at least 0.15 (see figure $7 a$ of Kerr \& Tait 1985). Both textural and isotopic evidence suggests that porosities were typically small in the Bushveld (Wager \& Brown 1968; Campbell 1987), which is consistent with the generally flat contact (with very gentle 'dimples') at the base of the Merensky Reef. Parts of the Reef are however disrupted by large 'potholes' (Campbell 1986; Ballhaus 1988). These potholes appear to be related to fluids released during the metamorphism of sediments underlying the Bushveld: such fluids could lead either to larger porosities in parts of the floor, or to the formation of deep 'fumeroles' in the floor that the replenishing magma is able to penetrate. For fumeroles to be important, flow velocities within them must be greater than the dissolving velocity of the interface, a condition that is satisfied if their diameters are greater than about $40 \mu \mathrm{~m}$ (assuming a magma viscosity $\mu$ of $300 \mathrm{~g} \mathrm{~cm}^{-1} \mathrm{~s}^{-1}$ and a density difference $\rho_{U}-\rho_{L}$ of $0.05 \mathrm{~g} \mathrm{~cm}^{-3}$ ).

### 4.2. The Rhum Intrusion

The Rhum Intrusion in Northwest Scotland is another location where the magma chamber has undergone many replenishments with dense picritic magma (Wager \& Brown 1968). At the contact between cyclic units 11 and 12 of this intrusion, Young (1984) observed several structural features (a dimpled contact, potholes, and an
intervening chrome-spinel layer) which he interpreted as being due to dissolution of the chamber floor after its replenishment. The floor at this time consisted of about $85 \%$ plagioclase, $10 \%$ augite and $5 \%$ olivine (Wager \& Brown 1968, pp. 268, 287), which has a fractionation density of about $2.55 \mathrm{~g} \mathrm{~cm}^{-3}$ (Sparks \& Huppert 1984) and a latent heat of about $1100 \mathrm{~J} \mathrm{~cm}^{-3}$. Using the compositions given by Tait (1985) for the replenishing and resident magmas, together with his estimate that the magmas contained about $1 \mathrm{wt} \%$ water, the density of the superheated mixed magma can be estimated to be about $2.67 \mathrm{~g} \mathrm{~cm}^{-3}$, which implies a buoyancy ratio of about 2.9. This value of the buoyancy ratio is large enough for dissolution to be driven by vigorous compositional convection, at rates similar to that estimated by (23) for the Bushveld anorthosite.

In dramatic contrast with the contact between units 11 and 12 , the contact between units 10 and 11 does not show similar evidence of dissolution after this previous replenishment of the magma chamber. This observation can be understood by noting that the upper part of unit 10 consists of about $55 \%$ plagioclase, $25 \%$ augite and $20 \%$ olivine (Wager \& Brown 1968, pp. 268, 272; Tait 1985, p. 472). This gabbroic assemblage has a much larger fractionation density (about $2.65 \mathrm{~g} \mathrm{~cm}^{-3}$ ), which results in a buoyancy ratio ( $\mathscr{R} \approx 0.5$ ) that is far too small to support vigorous compositional convection and significant dissolution. The upper 10 m of the gabbro is however enriched in magnesium, which suggests that the floor was porous enough to allow limited convective exchange between the interstitial and overlying magmas (Tait 1985; Kerr \& Tait 1985).

## 5. Conclusions

In this paper I have examined the dissolution of a solid that has been placed in contact with a solution whose composition is different to that of the solid. During the dissolution, the liquid at the interface will have a temperature and composition that are intermediate between that of the solid and that of the solution. The interfacial fluid will therefore have a different density to that of the solution, and in many situations this will give rise to convective motions (Woods 1992). The current paper investigates the simple case where the dissolving occurs at a horizontal floor or roof, and is driven by vigorous compositional convection. A scaling analysis was used to derive theoretical expressions for both the rate of dissolution and the interfacial concentration.

Experiments were then performed in which an ice roof or floor was dissolved in contact with aqueous solutions. The measured dissolving velocities are consistent with the scaling theory, and also suggest that the rate of dissolving is enhanced by the pitted nature of the interface and by the release of a significant heat of solution.

The results of this study are likely to have a diverse range of applications. One such application to replenished magma chambers has been examined, where dissolution velocities of a few centimetres per year are predicted. In many applications, the geometry of the solid will be more complicated than the simple one-dimensional case considered here (e.g. Kerr 1995). These situations will require further theoretical, experimental and numerical studies, but should be assisted by the physical understanding gained from the current work.

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## Appendix. The transition from dissolving to melting

When $\mathscr{C} \ll 1$, rapid movement of the interface (i.e. $V \gg D / h_{C}$ ) will result in a very nonlinear compositional profile, which is approximately given by

$$
\begin{equation*}
C(z) \approx C_{i}+\left(C_{f}-C_{i}\right) \mathrm{e}^{-V\left(h_{C}+z\right) / D}, \quad \text { where } \quad 0>z>-h_{C} \tag{A1}
\end{equation*}
$$

The resulting compositional flux $F_{C}$ to the interface is

$$
\begin{equation*}
F_{C} \approx V\left(C_{f}-C_{i}\right) \mathrm{e}^{-V h_{C} / D} \tag{A2}
\end{equation*}
$$

which when equated to ( $4 a$ ) yields

$$
\begin{equation*}
V \approx\left(D / h_{C}\right) \ln (1 / \mathscr{C}) \tag{A3}
\end{equation*}
$$

In this limit of rapid interfacial movement, the boundary layer estimates that were given by ( $8 a-c$ ) are now replaced by

$$
h_{C} \sim\left(\frac{P V \mu_{i}}{g\left(\rho_{f}-\rho_{i}\right)}\right)^{1 / 2}, \quad h_{T} \sim\left(\frac{P \mu_{i} \kappa_{f}^{2}}{g V\left(\rho_{f}-\rho_{i}\right)}\right)^{1 / 4}, \quad \tau \sim\left(\frac{P \mu_{i}}{g V\left(\rho_{f}-\rho_{i}\right)}\right)^{1 / 2} \quad(\mathrm{~A} 4 a-c)
$$

(see equations (3), (4) and (6) of Kerr 1994). Substitution of (A 4a) into (A 3) then results in the asymptotic law

$$
\begin{equation*}
V \sim\left(\frac{g\left(\rho_{f}-\rho_{i}\right) D^{2}}{P \mu_{i}}\right)^{1 / 3} \ln ^{2 / 3}\left(\frac{1}{\mathscr{C}}\right) \tag{A5}
\end{equation*}
$$

which is analogous to equation (A 5) of Kerr (1994). A combination of (A 5), (A 4b), (3b), (4b) and (1) then gives an expression for $C_{i}$ :

$$
\begin{equation*}
T_{f}-T_{L}\left(C_{i}\right) \sim \frac{\rho_{\varepsilon} L_{s}+\rho_{s} c_{s}\left(T_{L}\left(C_{i}\right)-T_{s}\right)}{\rho_{f} c_{f}}\left(\frac{D}{\kappa_{f}}\right)^{1 / 2} \ln ^{1 / 2}\left(\frac{1}{\mathscr{C}}\right) \tag{A6}
\end{equation*}
$$

If a Stefan number is defined by

$$
\begin{equation*}
\mathscr{S}_{i}=\frac{\rho_{s} L_{s}+\rho_{s} c_{s}\left(T_{i}-T_{s}\right)}{\rho_{f} c_{f}\left(T_{f}-T_{i}\right)} \tag{A7}
\end{equation*}
$$

(A 5) and (A 6) can be alternatively written as

$$
\begin{equation*}
V \sim\left(\frac{g\left(\rho_{f}-\rho_{i}\right) \kappa_{f}^{2}}{P \mu_{i} \mathscr{S}_{i}^{4}}\right)^{1 / 3} \tag{A8}
\end{equation*}
$$

and

$$
\begin{equation*}
\mathscr{S}_{i} \sim\left(\kappa_{f} / D\right)^{1 / 2} \ln ^{-1 / 2}(1 / \mathscr{C}) . \tag{A9}
\end{equation*}
$$

Equations (A 5) and (A 8) can then be viewed as providing the link between the dissolving expressions given by (9) and (14), which provide accurate upper and lower bounds on $V$ when $\mathscr{C}$ is large, and the melting expression given by equation (10) of Kerr (1994), which holds when $\mathscr{C} \approx 0$ and $T_{i} \approx T_{m}=T_{L}\left(C_{s}\right)$. Equation (A 9) can also be compared with the dissolving equations (10) and (15), which can be expressed respectively as $\mathscr{S}_{i}=\left(\kappa_{f} / D\right)^{1 / 2} \mathscr{C}$ and $\mathscr{S}_{i}=\left(\kappa_{f} / D\right)^{1 / 2}(\mathscr{C}+1)$.

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